## Selective and Direct Formation of Ethene from CO and $H_2$ over $In_2O_3-Y_2O_3$ , $-La_2O_3$ , and $-CeO_2$ Catalysts

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Ethene is selectively formed from CO and  $H_2$  over  $In_2O_3$ -containing oxide catalysts such as  $In_2O_3-Y_2O_3$ ,  $-La_2O_3$ , and  $-CeO_2$  at 673 K and 67 kPa with the highest selectivity of 43% for hydrocarbons.

Many studies on the selective synthesis of low molecular weight hydrocarbons from CO and  $H_2$  have been described. The selective syntheses of ethane,<sup>1</sup> propene,<sup>2,3</sup> n-butenes,<sup>4</sup> and isobutene<sup>5</sup> have been reported. However, the direct and selective synthesis of ethene has not been successful. We report here the marked effect that addition of In<sub>2</sub>O<sub>3</sub> to several oxides, such as Y<sub>2</sub>O<sub>3</sub>, La<sub>2</sub>O<sub>3</sub>, and CeO<sub>2</sub>, has in enhancing the selective formation of ethene.

In<sub>2</sub>O<sub>3</sub>-containing oxide catalysts (In<sub>2</sub>O<sub>3</sub>-Y<sub>2</sub>O<sub>3</sub>, -La<sub>2</sub>O<sub>3</sub>, and -CeO<sub>2</sub>) were prepared by co-precipitation from the aquous solution of each metal nitrate with NH<sub>4</sub>OH and calcination of the hydroxides at 773 K for 3 h. The atomic ratios of In to M (M = Y, La, and Ce) were 1:10. The oxide catalysts (Y<sub>2</sub>O<sub>3</sub>, La<sub>2</sub>O<sub>3</sub>, and CeO<sub>2</sub>) were prepared from the aqueous solution of each metal nitrate by the same procedure. The catalysts were evacuated before the reactions at 973 K. The reactions were carried out in a closed gas-circulating reaction system at 673 K and 67 kPa (H<sub>2</sub>:CO = 3) initial pressure.

Table 1 shows the activities and selectivities for hydrocarbons formed from CO and H<sub>2</sub> over the oxides and In<sub>2</sub>O<sub>3</sub>containing oxide catalysts. The single oxide catalysts  $(Y_2O_3,$  $La_2O_3$ , and  $CeO_2$ ) produce mainly branched-chain  $C_4$  and  $C_5$ hydrocarbons.<sup>6</sup> However, the addition of In<sub>2</sub>O<sub>3</sub> to these oxides results in an increase in the selectivity for ethene and a decrease in  $C_4$ ,  $C_5$ , and  $C_{6+}$  hydrocarbons. In<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> exhibits the highest selectivity for ethene formation (43%) and the highest activity for hydrocarbon formation at 673 K. The In<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> catalyst was stable for more than 48 h with a good carbon mass balance. When a mixture of H<sub>2</sub> and CO, ratio  $H_2: CO = 50$ , is introduced over  $In_2O_3$ -CeO<sub>2</sub>, the selectivity of ethene formation is still high, while the formation of methane increases. In contrast, the CO-H<sub>2</sub> reaction over In<sub>2</sub>O<sub>3</sub> alone, which was reduced to metallic indium under the reaction conditions, proceeds to form a large amount of CO<sub>2</sub> instead of hydrocarbons.

From results of X-ray photoelectron spectroscopy (XPS)

Catalysts	B.E.T.ª surface area	Activity <sup>b</sup>		Selectivity in hydrocarbons (carbon-base %)								Alkenec
		Hydrocarbon	CO <sub>2</sub>	CH4	$C_2H_4$	$C_2H_6$	$C_3H_6$	$C_3H_8$	C4	C <sub>5</sub>	C <sub>6+</sub>	selectivity
$Y_2O_3$	51	18 (0.35)	30	10	3	1	6	1	30	23	26	75
$In_2O_3 - Y_2O_3$	47	18 (0.38)	15	5	19	0.2	22	0.2	34	13	7	99
La <sub>2</sub> O <sub>3</sub>	17	9 (0.53)	18	15	3	4	5	3	19	21	29	43
$In_2O_3-La_2O_3$	17	12 (0.71)	14	7	31	3	15	1	20	16	7	92
CeO <sub>2</sub>	21	43 (2.0)	34	25	28	1	8	1	21	8	8	96
In <sub>2</sub> O <sub>3</sub> -CeO <sub>2</sub>	28	160 (5.7)	130	24	43	0.5	9	0.5	13	7	2	99
In <sub>2</sub> O <sub>3</sub> -CeO <sub>2</sub> <sup>d</sup>	28	21 (0.75)	4	48	42	0.5	7	0.3	2	0.2	+	99
In <sub>2</sub> O <sub>3</sub> e		trace	200			~~~~						

Table 1. Activity and selectivity for the  $CO-H_2$  reaction over oxide and  $In_2O_3$ -containing oxide catalysts.

<sup>a</sup> Brunauer-Emmett-Teller, m<sup>2</sup>/g. <sup>b</sup> The values are the average from the initial 2.5 to 17.5 h in carbon-base (µmol g-cat<sup>-1</sup> h<sup>-1</sup> and parentheses show activity based on specific surface area in carbon-base (µmol) m<sup>-2</sup> h<sup>-1</sup>. <sup>c</sup> C<sub>2</sub>H<sub>4</sub>/(C<sub>2</sub>H<sub>4</sub> + C<sub>2</sub>H<sub>6</sub>) ×100. <sup>d</sup> 50 kPa and H<sub>2</sub>/CO = 50. <sup>c</sup> In<sub>2</sub>O<sub>3</sub> was reduced to metallic indium under the reaction conditions.

measurements of  $In_2O_3$ - $Y_2O_3$ ,  $-La_2O_3$ , and  $-CeO_2$  after the reaction, the binding energies of In  $3d_{5/2}$  corrected by reference to Au  $4f_{7/2}$  (83.8 eV) were observed in the range 444.4---444.5 eV which are noticeably higher than the value of 443.3 eV for metallic indium.† These results indicate that  $In_2O_3$  supported on the oxides is not reduced to the metallic state under the reaction conditions. It was also found that the surface atomic ratios of In to M (M = Y, La, and Ce) by XPS were close to values for the bulk composition. The X-ray diffraction (XRD) patterns of  $In_2O_3$ -containing catalysts showed only the support oxides:  $Y_2O_3$  (cubic),  $La_2O_3$  (hexagonal), and CeO<sub>2</sub> (cubic). These results suggest that indium oxide is highly dispersed and this state probably has a

direct bearing on the highly selective formation of ethene. Similar results were obtained over  $Ga_2O_3$ -containing oxide catalysts.

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<sup>&</sup>lt;sup>†</sup> Commercial metallic indium (99.99%, Mitsuwa Co.) was spattered by Ar ion before the measurement, and the binding energy obtained for In  $3d_{5/2}$  was in good agreement with previous results.<sup>7</sup>